

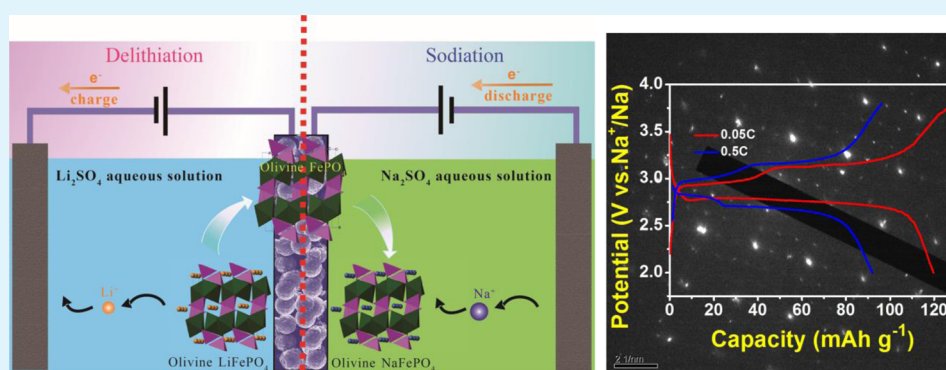
High-Performance Olivine NaFePO_4 Microsphere Cathode Synthesized by Aqueous Electrochemical Displacement Method for Sodium Ion Batteries

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S Supporting Information



ABSTRACT: Olivine NaFePO_4/C microsphere cathode is prepared by a facile aqueous electrochemical displacement method from LiFePO_4/C precursor. The NaFePO_4/C cathode shows a high discharge capacity of 111 mAh g^{-1} , excellent cycling stability with 90% capacity retention over 240 cycles at 0.1 C, and high rate capacity (46 mAh g^{-1} at 2 C). The excellent electrochemical performance demonstrates that the aqueous electrochemical displacement method is an effective and promising way to prepare NaFePO_4/C material for Na-based energy storage applications. Moreover, the $\text{Na}_{2/3}\text{FePO}_4$ intermediate is observed for the first time during the Na intercalation process through conventional electrochemical techniques, corroborating an identical two-step phase transition reaction both upon Na intercalation and deintercalation processes. The clarification of the electrochemical reaction mechanism of olivine NaFePO_4 could inspire more attention on the investigation of this material for Na ion batteries.

KEYWORDS: NaFePO_4 , olivine structure, aqueous, electrochemical displacement, Na ion batteries

1. INTRODUCTION

Rapid growth of renewable electricity requires low-cost electric energy storage (EES) devices for suppressing the impact of intermittent power on the electric grid. Although Li ion batteries (LIBs) are recognized as one of the most effective EES systems, concerns over the cost and continued availability of Li reserves have so far hindered its practical implementation for grid-scale energy storage application.^{1–3} In this regard, Na ion batteries (SIBs), sharing a similar chemistry with LIBs, have attracted extensive investigation, due to the greater abundance and lower cost of Na resources compared to Li.^{4–7}

A large variety of phases used in Li ion intercalation chemistry have been investigated as drop-in replacements for Na ion, including layered transition metal oxide O3- or P2- NaMO_2 ,^{8–11} orthorhombic $\text{Na}_{0.44}\text{MnO}_2$,^{12,13} phosphate polyanions,^{14–20} and so on. Due to the much larger size, Na ion mobility in the cubic closed-packed oxide arrays is sluggish; the Na ion intercalation/deintercalation often results in very complicated phase transitions, leading to rapid structural

degradation of the hosts upon cycling. From the structural point of view, open frameworks are more suitable to host the large-sized guest Na ions. For example, Prussian blue type materials have a cubic open framework capable of rapid and reversible Na ion movement, despite suffering from low specific capacity (about 100 mAh g^{-1}).^{21–23} NASICON-type $\text{Na}_3\text{V}_2(\text{PO}_4)_3$, as one of the Na-superion conductors, has been demonstrated to have faster Na ion diffusion coefficient than its Li analogues.^{19,24–26} Mixed transition metal maricite ($\text{NaMn}_{1/3}\text{Co}_{1/3}\text{Ni}_{1/3}\text{PO}_4$) has also been investigated as electrode materials and showed decent capacitor performance with 405 F g^{-1} over 1000 cycles.²⁷ However, the use of iron-based phosphates as host materials will be advantageous with regard to cost-effectiveness and environmental friendliness.^{17,18,28,29} Among the series of iron phosphates, olivine

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NaFePO₄ possesses the highest theoretical specific capacity (154 mAh g⁻¹) and decent working voltage, which make it attractive as a host material for Na ions.^{28,30–32}

NaFePO₄ obtained from direct high-temperature synthesis usually presents a thermodynamically favored maricite phase, which has no free channels for Na ion diffusion in the closed framework.^{18,33} Le Poul first found that the guest Li ions in the olivine iron phosphate host can be replaced by Na ions.³⁴ Afterward, olivine NaFePO₄ was frequently accessed via chemical or electrochemical displacement methods from olivine LiFePO₄ in organic solutions.^{20,28,30–32} Oh et al. reported olivine NaFePO₄ prepared by electrochemical Li–Na exchange from LiFePO₄ with a stable capacity of 125 mAh g⁻¹ at a current rate of 0.05 C.²⁸ Zhu et al. conducted a comparative study of the electrochemical performances of olivine NaFePO₄ in SIBs and olivine LiFePO₄ in LIBs and attributed the poorer performances of olivine NaFePO₄ to the lower diffusion coefficient of Na ions and higher charge transfer resistance in NaFePO₄ cathodes.³¹ Meanwhile, the Na ion intercalation/deintercalation mechanism was thoroughly scrutinized.^{35–37} Contrary to the direct biphasic reaction in micrometric LiFePO₄, a handful of research studies have found that Na ion intercalation/deintercalation underwent an intermediate phase close to Na_{0.7}FePO₄, which was recently identified to be an ordered Na_{2/3}FePO₄ composition.^{32,35–38} The Na ion deintercalation from NaFePO₄ first went through a solid solution domain until the formation of Na_{2/3}FePO₄ phase and then proceeded through a two-phase process to form olivine FePO₄, which was characterized by two voltage plateaus on the charge profiles. The Na ion intercalation into olivine FePO₄ was reported to be different from the reversed Na ion deintercalation process.^{32,35,36} Casas-Cabanas et al. reported the simultaneous existence of three phases: FePO₄, Na_{2/3}FePO₄, and NaFePO₄.^{35,38} A single plateau was mostly observed on discharge profiles.^{28,30–32,35,36,38} The asymmetric Na ion intercalation/deintercalation mechanism was generally ascribed to the larger volumetric mismatch between NaFePO₄ and FePO₄ (17.58% difference in unit volume) compared to only 6.9% for their Li counterparts.^{35,38}

Previous works have shown that olivine LiFePO₄ can be reversibly (de)lithiated in aqueous solution, exhibiting fast diffusion kinetics as well as good cycling performance.^{39,40} In aqueous SIBs, fast transport of Na ions has already been verified.^{12,41,42} By analogy, it can be expected that NaFePO₄ could also undergo reversible sodiation in aqueous solution. Minakshi and Meyrick have shown that the maricite (NaMn_{1/3}Co_{1/3}Ni_{1/3}PO₄) is electrochemically active when using an aqueous NaOH electrolyte.⁴² Recently, Vujković and Mentus reported a direct transformation from LiFePO₄ to NaFePO₄ in saturated NaNO₃ solution by cyclic voltammetry,⁴³ clearly proving the feasibility of electrochemical synthesis of NaFePO₄ via aqueous medium. Herein, we report a facile synthesis of olivine NaFePO₄ by aqueous electrochemical displacement of Li ions from olivine LiFePO₄ by Na ions. This displacement process is quick, easy, cost-saving, and green compared to that in organic electrolyte, and the thus-obtained NaFePO₄ cathode shows high reversible capacity and cycle performance in SIBs. Moreover, we reveal, for the first time, that the Na ion intercalation/deintercalation can proceed in a reversible two-step phase transition reaction and a clear phase separation is determined by reaction rate.

2. EXPERIMENTAL SECTION

2.1. Material Synthesis and Electrode Preparation. All of the reagents were purchased from Alfa Aesar without further purification. LiFePO₄/C microsphere precursor was prepared by a template-free hydrothermal process as described in our previous work.⁴⁴ Stoichiometric amounts of CH₃COOLi·2H₂O, Fe(NO₃)₃·9H₂O, NH₄H₂PO₄, and citric acid (mole ratio is 1:1:1:1) were dissolved in deionized water to form a transparent solution of 70 mL. The solution was then transferred into a 100 mL Teflon-lined stainless steel autoclave and maintained at 180 °C for 6 h. Afterward, the hydrothermal product was mixed with an appropriate amount of sucrose, dehydrated at 80 °C overnight, and then calcined at 650 °C for 10 h in a 5% H₂/Ar atmosphere to obtain the LiFePO₄/C microspheres.

The LiFePO₄ electrode was prepared by roll-pressing the thoroughly mixed paste of 80 wt % LiFePO₄/C, 10 wt % acetylene black, and 10 wt % polytetrafluoroethylene into a thin film (~5 mg cm⁻²) and pressing the film onto a Ti mesh.

The NaFePO₄ electrode was obtained by a two-step aqueous electrochemical transition process. The aqueous cell has a three-electrode design, with LiFePO₄ electrode (~1 cm²) as working electrode, activated carbon electrode as counter electrode, and Ag/AgCl electrode (0.197 V vs NHE) as reference electrode. The three electrodes were first inserted into 1 mol L⁻¹ Li₂SO₄ aqueous solution and fully charged (delithiated) to 0.7 V with a current rate of 17 mA g⁻¹. Then, the three electrodes were thoroughly rinsed with deionized water, transferred into 1 mol L⁻¹ Na₂SO₄ aqueous solution, and fully discharged (sodiated) to -0.6 V at a current of 17 mA g⁻¹ to achieve an olivine NaFePO₄ electrode. The NaFePO₄ electrode was also rinsed with deionized water and dried at 70 °C in vacuum overnight for use.

2.2. Characterization. X-ray powder diffractions were obtained by using a Shimadzu XRD-6000 diffractometer with Cu Kα. The data were recorded in the 2θ range of 15–60° with a scan rate of 4° min⁻¹ at a step size of 0.02°. The morphologies of the materials were observed by SEM (Merlin Compact FE-SEM, Zeiss) and TEM (JEM-2100F). The element dispersive spectroscopy (EDS) mapping of the composite was obtained from an oxford detector (X-Max^N, Oxford) attached to the SEM. The selected electron diffraction was obtained by TEM with the operated potential set at 200 kV. The carbon content in the LiFePO₄/C microspheres was analyzed by CHNS Vario EL cube (Elementar Analysen Systeme GmbH, Hanau, Germany).

2.3. Electrochemical Measurements in Organic Electrolyte. The electrochemical cells were assembled into CR2016-type coin cells, with NaFePO₄ electrode as cathode, Na thin disk as anode, cellogard 2035 as separator, and 1.0 mol L⁻¹ NaPF₆ dissolved in ethylene carbonate/diethyl carbonate (EC/DEC, 1:1 by volume) as electrolyte. The cell assembly was carried out in a glovebox with water/oxygen content lower than 0.5 ppm, and the loading mass of the active material was ~4 mg cm⁻². The room temperature constant current discharge/charge tests were conducted on a LAND cyler (Wuhan Kingnuo Electronic Co., Wuhan, China). Cyclic voltammetry measurements were performed on a CHI 660a electrochemical workstation (ChenHua Instruments Co., Shanghai, China).

3. RESULTS AND DISCUSSION

3.1. Synthesis and Characterization of the NaFePO₄/C Microsphere. LiFePO₄/C microsphere precursor was prepared by a template-free hydrothermal process as described in our previous work.⁴⁴ The SEM and TEM images of the product are shown in Figure 1. It shows that the product appears as micrometer-sized spheres with a quite uniform diameter of ~3.5 μm (Figure 1a,c). The enlarged image of a single microsphere shows that it was composed of densely aggregated nanoparticles and has a porous structure (Figure 1b). This peculiar structure should favor electrolyte infiltration as well as obtain high tap density. The carbon content in the product was evaluated to be 2.8% by element analysis. The LiFePO₄/C microsphere electrode demonstrated excellent Li ion inter-

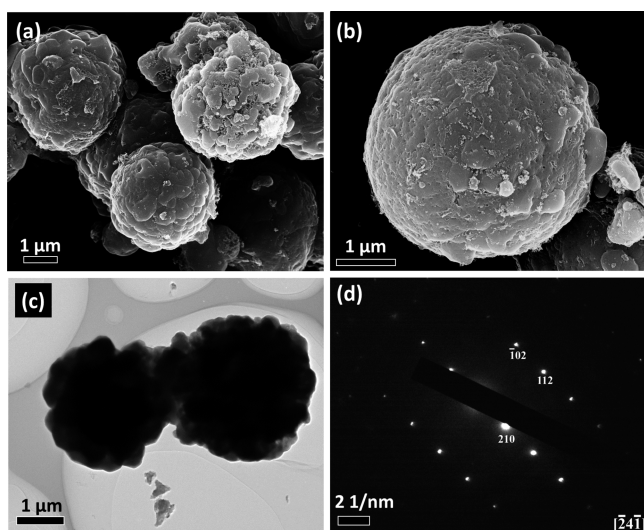


Figure 1. SEM (a and b) and TEM (c) images and SAED pattern (d) of the LiFePO_4/C microspheres precursor.

calation/deintercalation electrochemical performance in both organic and aqueous systems as shown in Figure S1 (see Supporting Information (SI)), guaranteeing a highly structure-stable architecture to be used for making NaFePO_4/C .

The synthetic scheme of the olivine NaFePO_4/C through an aqueous electrochemical displacement is illustrated in Figure 2.

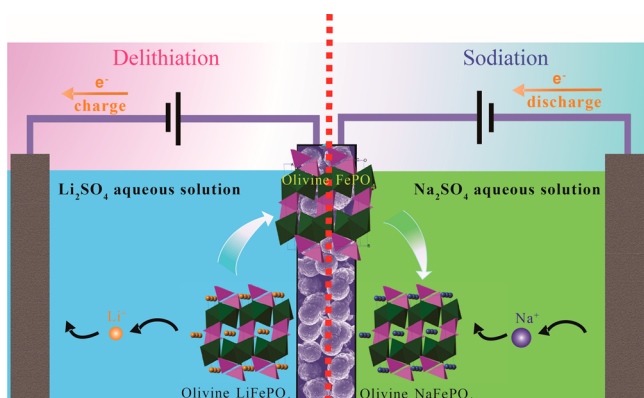


Figure 2. Synthetic scheme of the aqueous electrochemical displacement process from olivine LiFePO_4 to isostructural NaFePO_4 .

First, the olivine LiFePO_4/C electrode was fully delithiated (charged) in 1 mol L^{-1} Li_2SO_4 aqueous solution to get the isostructural FePO_4/C . After being washed thoroughly by deionized water, the FePO_4/C electrode was transferred into 1 mol L^{-1} Na_2SO_4 aqueous solution and then fully sodiated (discharged) to obtain the final olivine NaFePO_4/C electrode. The NaFePO_4/C electrode was then vacuum-dried for use.

Parts a and b of Figure 3 present the cyclic voltammetry (CV) and constant current charge–discharge illustrations demonstrating the direct electrochemical conversion from LiFePO_4/C to NaFePO_4/C in aqueous solutions, respectively. The aqueous cell has a three-electrode design, with LiFePO_4/C electrode as working electrode, activated carbon electrode as counter electrode, and Ag/AgCl electrode (0.197 V versus NHE) as reference electrode. Figure 3a gives the CV plots scanned at 1 mV s^{-1} . When first scanned positively in Li_2SO_4 aqueous solution from -0.3 to 0.7 V (denoted by blue solid

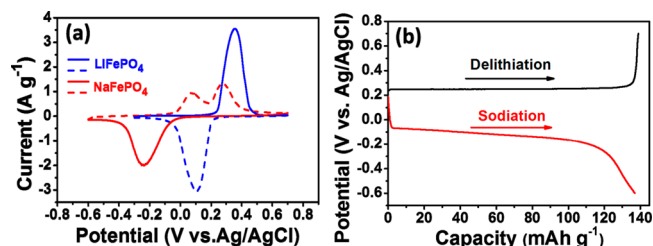


Figure 3. (a) Cyclic voltammetry and (b) constant current charge–discharge illustration of the aqueous electrochemical displacement process from olivine LiFePO_4 to FePO_4 in 1 mol L^{-1} Li_2SO_4 solution and then to NaFePO_4 in 1 mol L^{-1} Na_2SO_4 solution.

line), the electrode presents an intensive delithiation peak at 0.35 V . When the electrode was transferred into Na_2SO_4 aqueous solution and scanned negatively from 0.7 to -0.6 V (red solid line), a broad sodiation peak was observed at -0.25 V , exhibiting a successful displacement process of Li ions by Na ions. Figure 3a also gives the corresponding lithiation and desodiation processes as presented in dashed lines. The reversed lithiation of FePO_4/C occurs at 0.1 V (the blue dashed line in Figure 3a), and the reversed desodiation of NaFePO_4/C gives two peaks at 0.05 and 0.3 V (the red dashed line in Figure 3a). Based on the intervals of the redox peaks, it is apparent that LiFePO_4 shows faster reaction kinetics than NaFePO_4 in aqueous solution. Besides, the areas of the two desodiation peaks of NaFePO_4/C are estimated to be about 1:2. Obviously, the CV feature of NaFePO_4 in aqueous solution is quite similar to that observed from organic solution in refs 31 and 43 and our work shown later, indicating that the reaction mechanisms of NaFePO_4 in aqueous and organic systems are identical. Thus, it can be reasonably speculated that the two desodiation peaks originate from a two-step reaction process and are sequentially attributed to the desodiation of NaFePO_4 to $\text{Na}_{2/3}\text{FePO}_4$ intermediate phase, and then to FePO_4 .

Figure 3b gives the charge profile of the LiFePO_4/C electrode in Li_2SO_4 aqueous solution and the discharge profile in Na_2SO_4 aqueous solution cycled at 0.1 C ($1 \text{ C} = 170 \text{ mA g}^{-1}$ based on LiFePO_4). The LiFePO_4/C electrode presents a typical flat delithiation voltage profile at 0.25 V with a capacity of ca. 140 mAh g^{-1} , and a sloping sodiation plateau at -0.1 V with a capacity of 137 mAh g^{-1} , suggesting that almost all interstitial sites originally occupied by Li ions are taken over by Na ions through one discharge–charge process. SEM (Figure 4a,b,e) and TEM (Figure 4c) observation further revealed that the obtained NaFePO_4/C composites retained a microspherical structure. The corresponding elemental mappings of Na, Fe, P, and O are shown in Figure 4f–i, exhibiting a uniform element distribution in the microsphere. The EDS spectrum (Figure 4j) analysis shows that the Na/Fe/P/O ratio is nearly 1:1:1:4, indicating that the microsphere is NaFePO_4 .

What's more, Figure 5 gives the XRD patterns of the initiative LiFePO_4 samples fully charged to 0.7 V in Li_2SO_4 aqueous solution and fully discharged to -0.6 V in Na_2SO_4 aqueous solution. As can be seen, all of the XRD reflections can be well-indexed to a pure olivine phase respectively, indicating a very robust olivine framework constituted by FePO_4 . Thus, Figures 4 and 5 confirm that LiFePO_4 can be successfully transformed into NaFePO_4 through a two-step aqueous electrochemical process.

3.2. Electrochemical Measurement of the NaFePO_4/C Microsphere in Organic Electrolyte. The olivine NaFePO_4/C

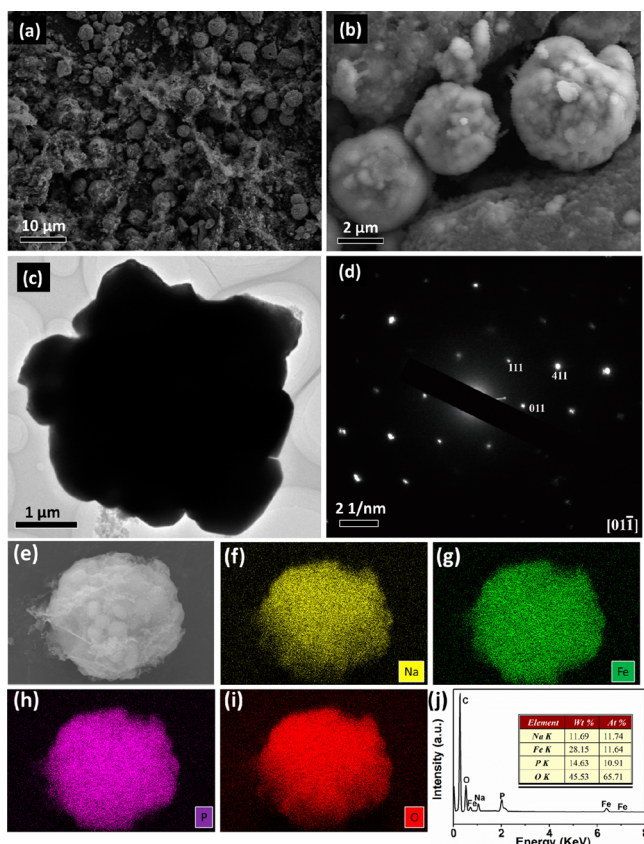


Figure 4. SEM (a and b) and TEM (c) images and SAED pattern (d) of the NaFePO₄/C microspheres converted electrochemically in aqueous solution; (e) typical SEM image of as-prepared NaFePO₄/C microsphere and the corresponding elemental mapping of sodium (f), iron (g), oxygen (h), and phosphorus (i), and EDS spectrum of the NaFePO₄/C microsphere (j; inset, element content of the mapping area).

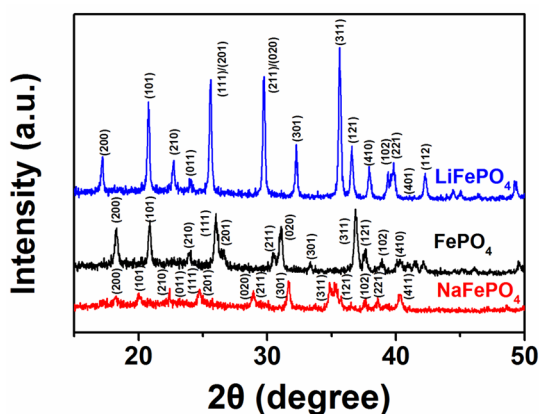


Figure 5. XRD patterns of the pristine LiFePO₄/C powder, the fully delithiated FePO₄/C electrode in 1 mol L⁻¹ Li₂SO₄ aqueous solution, and the final sodiated NaFePO₄/C electrode in 1 mol L⁻¹ Na₂SO₄ aqueous solution.

C electrode prepared by aqueous electrochemical displacement was assembled into coin cells with Na electrode and 1 mol L⁻¹ NaPF₆/EC:DEC (1:1 by volume) electrolyte. The electrochemical test results of the NaFePO₄/C electrodes are presented in Figure 6. The CV curve scanned at a rate of 0.05 mV s⁻¹ in Figure 6a shows two well-defined desodiation

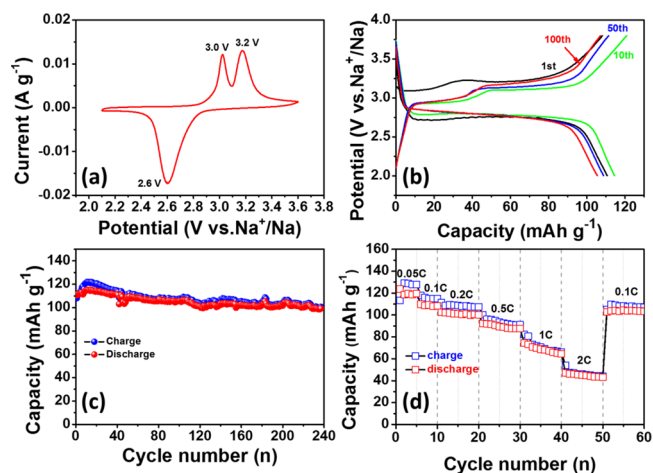


Figure 6. Electrochemical performance of the NaFePO₄/C cathode: (a) Cyclic voltammogram scanned between 2.1 and 3.6 V vs Na⁺/Na at a rate of 0.05 mV s⁻¹; (b) constant current charge/discharge profiles and (c) charge/discharge capacity versus cycle number at 0.1 C; (d) rate cycling performance at various rates from 0.05 to 2 C. The counter electrode was a Na disk electrode, and the electrolyte was 1.0 mol L⁻¹ NaPF₆/EC:DEC (1:1 by volume); the voltage window of charge/discharge was 2.0–3.8 V.

peaks and a single sodiation peak, in good accord with those reported in previous study.^{31,43} Figure 6b shows the charge–discharge profiles at different cycles at a current rate of 0.1 C (1 C = 154 mA g⁻¹). Over 100 cycles, two charge plateaus at 2.90 and 3.20 V and a single discharge plateau at 2.75 V are clearly distinguished. The voltage plateaus are reflected as redox peaks in the CV curves (Figure 6a). Two charge plateaus (or two oxidative peaks in the CV plot) correspond respectively to a two-phase reaction from NaFePO₄ to Na_{2/3}FePO₄ and a solid solution reaction from Na_{2/3}FePO₄ to FePO₄.^{32,35,36} One notes that the hysteresis between the charge–discharge voltage plateaus of NaFePO₄ is larger than that of LiFePO₄ in LIBs (Figure S1a), which might be caused by a higher energy difference during phase transition and slower intercalation kinetics in the olivine framework as well as larger charge transfer resistance for Na ions than for Li ions.³¹ The electrode first delivers a reversible capacity of 111 mAh g⁻¹ (Figure 6b), which is lower than that (137 mAh g⁻¹) obtained in aqueous electrolyte (Figure 3b) at the same discharge rate, indicating slower reaction kinetics in organic electrolyte due to lower ionic conductivity and higher viscosity of the organic electrolyte compared to in aqueous electrolyte. However, the NaFePO₄/C electrode reported here displays higher capacity for Na ion storage in the organic system than most of the previous works.^{18,28,31,38} Obviously, the charge profile of the first cycle is different from the subsequent cycles. The different charge profile appearing at the first cycle could be attributed to reconstruction of the surface layer between the material and electrolyte. As is well-known, the reaction interface structures between the material and electrolyte are different in aqueous and organic electrolytes. The surface film structure formed in aqueous electrolyte might be unsuitable for ionic diffusion through the interface during charging/discharging in organic electrolyte, thus leading to a larger polarization in the first cycle in organic electrolyte. Moreover, the NaFePO₄/C electrode displays almost overlapped charge–discharge profiles in the subsequent cycles, exhibiting excellent Na ion intercalation/deintercalation reversibility. As is shown in Figure 6c, the

electrode still attains a reversible capacity of 100 mAh g⁻¹ after 240 cycles, corresponding to a capacity retention ratio of 90%. The cycle capability greatly exceeds that of NaFePO₄ ever reported, as shown in Table S1. Additionally, the reversible capacity increase (the activation process) in the first 15 cycles is possibly due to a slow infiltration of electrolyte into the interior of the NaFePO₄/C microsphere, which creates gradually the electrochemically active interface. A similar increase in capacity during the initial cycles has also been observed for the LiFePO₄ materials in previous literature.^{45,46} The rate capability of NaFePO₄/C was also investigated as displayed in Figure 6d. The electrode achieves discharge capacities of 120, 109, 101, 92, 71, and 46 mAh g⁻¹ at the C-rates of 0.05, 0.1, 0.2, 0.5, 1, and 2 C, respectively, which are better than most of the previous reports so far.^{28,31}

The preceding test results are indicative of excellent electrochemical reversibility and rate capability of the NaFePO₄/C electrode developed in this work, superior to those synthesized by chemical or electrochemical oxidation/reduction reactions in organic solutions started from LiFePO₄ precursors. We believe that the aqueous electrochemical displacement method is advantageous owing to the very fast de(intercalation) kinetics of Li and Na ions in the aqueous solution. On this account, Li ions can be fully extracted from the lattice promoted by the potential field even at relatively large current rate. No Li ion residuals in the resulting FePO₄ lattice is very crucial to making sure there are more lattice sites and more fluent channels for Na ion intercalation. Fast reaction kinetics also brings about lower potential polarization so as to cause smaller structural deformation. Besides, aqueous solution would create less detriment to the structure of materials. In contrast, the chemical delithiation of LiFePO₄ using strong oxidizer such as NO₂BF₄ and bromine was found to create structural defects and amorphization due to the violent reaction.^{47,48} Therefore, the aqueous electrochemical displacement method not only provides an effective, easy, cost-saving, and green preparation route for olivine NaFePO₄ but also endows desirable electrochemical performance.

3.3. Study on Phase Transition during Electrochemical Reaction. Besides the pursuit of favorable synthesis means and honorable electrochemical performance with the olivine-type metallophosphate family, the scientific community also has particular interest in understanding the fundamental reaction mechanics accompanying the alkali metal de(intercalation). As is commonly observed in the host materials that suffer from huge volume change during de(intercalation), such as anatase TiO₂,⁴⁹ some layered intercalation compounds,⁵⁰ LiMnPO₄ (8.9% difference in unit volume),⁵¹ and even LiFePO₄ (only 6.9%),³⁸ the lattice structures would experience a stage transformation process to buffer the mechanical strain. This staging phenomenon also happens in NaFePO₄, due to the large volumetric mismatch between NaFePO₄ and FePO₄ (ca. 17.58% difference in unit volume). In previous research studies, the formation of an intermediate ordered Na_{2/3}FePO₄ superstructure was identified by various spectroscopic techniques,^{37,52} composition–temperature phase diagram,³⁶ and two plateaus on battery charging,^{32,35} so that two successive stage phase transformations from NaFePO₄ to Na_{2/3}FePO₄ and then to FePO₄ were reasonably established. However, the voltage profiles on battery discharge in previous observations only showed a single plateau, which was attributed to the fact that phase transformation from Na_{2/3}FePO₄ to NaFePO₄ (3.6% difference in volume) present much lower

kinetic barriers compared to that from FePO₄ to Na_{2/3}FePO₄ (13.5% difference in volume).^{35,38}

In the preceding rate capability experiment, we found an interesting phenomenon wherein a voltage profile evolution occurred with the acceleration of discharge rate. As is shown in Figure 7, the voltage profiles at low discharge rates of 0.05 and

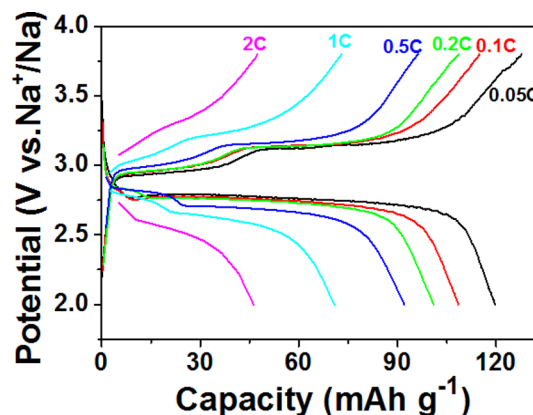


Figure 7. Voltage–capacity profiles of the NaFePO₄/C electrode at different charge/discharge rates from 0.05 to 2 C.

0.1 C show only a single discharge plateau, similar to the previous observations. However, as the current rate increases to ≥ 0.2 C, two distinct plateaus separated by a large voltage gap (0.1 V) appear. The distinct divide of the discharge plateaus indicates that a Na_{2/3}FePO₄ intermediate phase also forms upon sodiation process. To confirm the presence of the intermediate phase at high discharge rate, *ex situ* X-ray diffraction (XRD) was employed to characterize the phase transformation during the whole Na ion intercalation process in the FePO₄/C electrode. As presented in Figure S2, the XRD diffractions correspond to a FePO₄ phase at open circuit voltage. When discharged at 0.5 C to the end of the first voltage plateau around 2.75 V, a set of new XRD diffractions appear pointing out a discharge intermediate of Na_{2/3}FePO₄ phase.^{32,35,36,52} After full discharge to 2.0 V, all of the Na_{2/3}FePO₄ signals disappear again and the diffraction pattern can be indexed to a pure phase of NaFePO₄. Thus, the *ex situ* XRD measurement and discharge voltage profile corroborate that Na ion intercalation actually goes through a similar reaction path via a Na_{2/3}FePO₄ intermediate phase to the deintercalation process. Additionally, the TEM and selected area electron diffraction (SAED) pattern were also performed to confirm the presence of the Na_{2/3}FePO₄ intermediate as shown in Figure 8. The SAED pattern from the TEM images of the intermediate during discharging displayed the diffraction spots obtained along the [110] direction. Particularly, some superlattice spots (Figure 8a) can be observed apparently in the SAED pattern compared to the NaFePO₄ sample (Figure 4c). The superstructure is considered as the contribution of a Na ion pair and Fe^{II}/Fe^{III} charge ordering reported by previous literature, indicating the characteristics of the Na_{2/3}FePO₄ intermediate.^{37,38,52} Similar to Boucher's study,³⁷ the superlattice spots disappear after 1 min irradiation (Figure 8b), due to its instability when exposed to electron beam at room temperature. This phenomenon gives strong evidence to prove that the Na_{2/3}FePO₄ intermediate is indeed present during discharging. To the best of our knowledge, this is the first direct evidence of two successive stage phase transformation

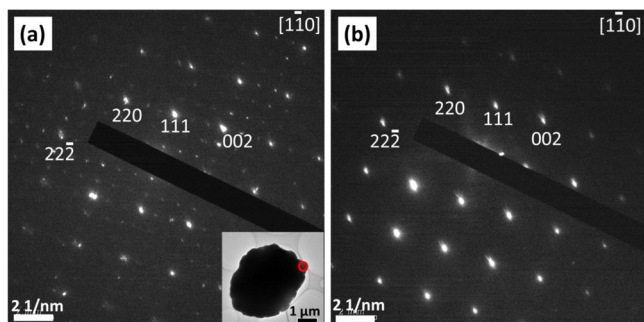
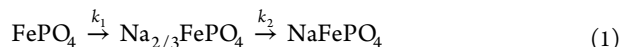


Figure 8. Selected electron diffraction patterns of the $\text{Na}_{2/3}\text{FePO}_4$ intermediate: (a) pattern obtained along the $[1\bar{1}0]_{Pnma}$ zone axis and (b) same position as a but after 1 min irradiation.

processes during Na ion intercalation into FePO_4 by means of constant current discharge. This discovery could adequately resolve the uncertainties in previous studies of whether $\text{Na}_{2/3}\text{FePO}_4$ intermediate phase is present during discharge.^{35,38}

3.4. Electrochemical Mechanism of Olivine NaFePO_4

Since the discharge process is two successive first order phase transformations via $\text{Na}_{2/3}\text{FePO}_4$ intermediate phase, the reaction can be written as follows:



k_1 and k_2 are the rate constants for the reaction from FePO_4 to $\text{Na}_{2/3}\text{FePO}_4$ and that from $\text{Na}_{2/3}\text{FePO}_4$ to NaFePO_4 , respectively. Because the unit volume expansion (13.5%) from FePO_4 to $\text{Na}_{2/3}\text{FePO}_4$ is more than 3 times larger than that (3.6%) from $\text{Na}_{2/3}\text{FePO}_4$ to NaFePO_4 , the first phase transformation should overcome a much higher kinetics barrier than the follow-up one; namely, $k_1 \ll k_2$. Therefore, at low reaction rates, $\text{Na}_{2/3}\text{FePO}_4$ formed from the first transformation process would transform into NaFePO_4 immediately. Thus, the apparent reaction looks like a direct transformation from FePO_4 to NaFePO_4 , as reflected by a single voltage plateau on discharge profiles. At high reaction rates otherwise, the high electrochemical overpotential greatly accelerates the first transformation, which becomes even comparative to the subsequent one; the apparent reaction would exhibit a two-step phase transformation, corresponding to two voltage plateaus on the discharge curves. However, it should be addressed that, in the charge process, whether at low or high rates, NaFePO_4 would always transform into $\text{Na}_{2/3}\text{FePO}_4$ at first, which then transforms into FePO_4 ($k_2 \gg k_1$), so that the charge would always exhibit a two-step phase transformation process (two voltage plateaus).

To verify the preceding discussion, cyclic voltammetry was reconstructed on the NaFePO_4/C electrode at high scan rates of 0.5, 1, and 2 mV s^{-1} as presented in Figure 9. As expected, two well-defined reductive peaks emerge at high scan rates compared to one reductive peak at 0.05 mV s^{-1} (Figure 6a). The current peaks in the CV curves are in good accord with the discharge plateaus at high rates (Figure 7). Because cyclic voltammetry is a transient method, it can capture a short-lifetime reaction intermediate by regulating the scan rates. Because k_1 is much smaller than k_2 in eq 1, $\text{Na}_{2/3}\text{FePO}_4$ would transform into NaFePO_4 immediately as soon as it is produced during slow scan. Therefore, the concentration of $\text{Na}_{2/3}\text{FePO}_4$ intermediate in the system is very low and cannot be captured by CV. As the scan rate expedites, the concentration of the intermediate would accumulate to be detected. Consequently, a

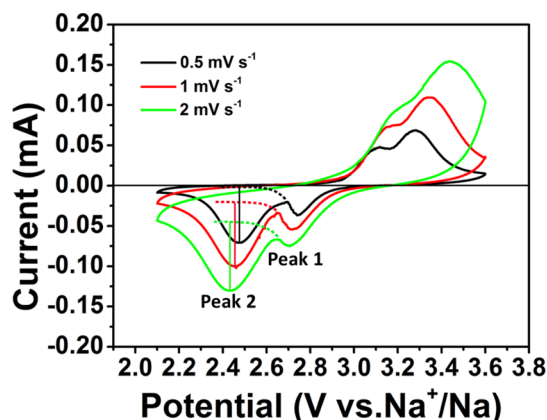


Figure 9. Cyclic voltammograms of NaFePO_4/C electrode in 1 mol L^{-1} $\text{NaPF}_6/\text{EC}:\text{DEC}$ (1:1 in vol) solution at various scan rates.

reductive peak derived from the fast reaction (k_2) would split away from the primary single peak. Thus, the CV results further verify the existence a $\text{Na}_{2/3}\text{FePO}_4$ intermediate during Na intercalation process, and a two-step phase transformation process occurs both on Na intercalation and deintercalation. Obviously, this reaction rate dependent $\text{Na}_{2/3}\text{FePO}_4$ appearance is in fact rooted from the disparity of k_1 and k_2 .

According to Bard's book,⁵³ the peak current i_p has a relationship with the peak potential E_p as displayed by the following equation:

$$i_p = 0.227nFAC_0^*k^0 \exp[-af(E_p - (E^0)')] \quad (2)$$

where $(E^0)'$ is the formal potential for the reduction. For a multistep charge transfer reaction, the peak current (i_p) in the $i-E$ curve is the sum of the individual $i-E$ curves of FePO_4 and $\text{Na}_{2/3}\text{FePO}_4$. In this regards, the measurement of i_{p2} must be made using the decaying current of the first wave as the baseline. The values of i_{p2} are corrected correspondingly as shown in Figure 9, and the related parameters of eq 1 are shown in Table S2.

According to eq 2, a plot of $\ln i_p$ vs $E_p - (E^0)'$ determined at different scan rates should have a slope of $-af$ and an intercept proportional to k^0 ; namely,

$$\ln i_p = -af(E_p - (E^0)') + \ln(0.227nFAC_0^*k) \quad (3)$$

Considering peak 1 and peak 2, we get the different lines as shown in Figure 10. At 25 °C, for $F = 96485.4 \text{ C mol}^{-1}$, A is $\pi^2/6 = 0.13083 \text{ cm}^2$, $C_{10}^* = C_{20}^* = 1 \text{ mol L}^{-1}$, $n = 2/3$ for k_1 or $1/3$ for k_2 , and the values of k_1 and k_2 are deduced to be $1.21 \times 10^{-6} \text{ cm s}^{-1}$ and $2.43 \times 10^{-5} \text{ cm s}^{-1}$ based on eq 3 and the corresponding intercept obtained from Figure 10, respectively. Clearly, k_2 corresponding to the reaction from $\text{Na}_{2/3}\text{FePO}_4$ to

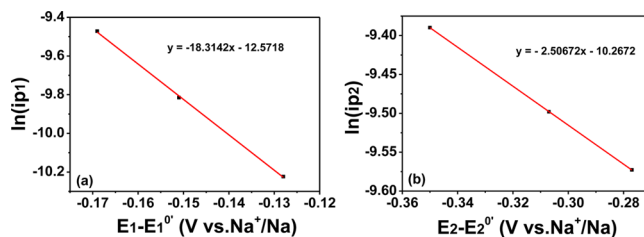


Figure 10. Plot of $\ln i_{p1}$ vs $E_{p1} - (E^0)'$ (a) and plot of $\ln i_{p2}$ vs $E_{p2} - (E^0)'$ (b) determined at different scan rates.

NaFePO₄ is about 20-fold higher than k_1 for the reaction from FePO₄ to Na_{2/3}FePO₄. This result further demonstrates the preceding discussion, which is an identical two-step phase transition reaction upon Na intercalation and deintercalation processes.

4. CONCLUSIONS

In summary, olivine NaFePO₄/C cathode was prepared by a facile aqueous electrochemical displacement method from olivine LiFePO₄/C precursor. The NaFePO₄/C cathode displays a high discharge capacity of 111 mAh g⁻¹ along with 90% capacity retention over 240 cycles at 0.1 C and high rate capacity (46 mAh g⁻¹ at 2 C). The excellent electrochemical performance demonstrates that the electrochemical displacement method offers an inexpensive, effective, and promising approach to prepare NaFePO₄/C materials for Na-based energy storage applications. Of particular significance is that we first observe the appearance of Na_{2/3}FePO₄ intermediate during Na intercalation process with conventional electrochemical techniques, corroborating an identical two-step phase transition reaction upon Na intercalation and deintercalation processes. The clarification of the electrochemical reaction mechanism could also inspire more attention on the development of high-performance NaFePO₄ material.

■ ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acsami.5b04691.

Electrochemical characterization of the LiFePO₄/C electrode, charge/discharge curves of the NaFePO₄/C and corresponding XRD patterns of the NaFePO₄/C electrode at different discharge depths, comparison of the cycle performance of the olivine NaFePO₄ electrode, and measured and calculated data based on the i - E curves of the NaFePO₄/C electrode (PDF).

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Notes

The authors declare no competing financial interest.

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